

STEADY STATE RESULTS FOR CLOSEDLOOP

i.e. constant input file and ideal sensors/actuators, control strategy according to BSM1 description

(Results from Matlab/Simulink implementation by Dr Ulf Jeppsson, IEA, Lund University, Sweden, May 21 2009 – based on Matlab R2008b (ver 7.7.0))

Influent characteristics

SI = 30 mg COD/l
SS = 69.5 mg COD/l
XI = 51.2 mg COD/l
XS = 202.32 mg COD/l
XBH = 28.17 mg COD/l
XBA = 0 mg COD/l
XP = 0 mg COD/l
SO = 0 mg -COD/l
SNO = 0 mg N/l
SNH = 31.56 mg N/l
SND = 6.95 mg N/l
XND = 10.59 mg N/l
SALK = 7 mol HCO₃/m³
TSS = 211.2675 mg SS/l

Flow conditions

Influent flow to WWTP = 18446 m³/d
Influent flow to AS = 53377.6075 m³/d
Internal recirculation = 16485.6075 m³/d
Settler feed flow = 36892 m³/d
Returned sludge flow = 18446 m³/d
Wastage sludge flow = 385 m³/d
Effluent flow = 18061 m³/d

Input to AS

SI = 30 mg COD/l
SS = 24.5463 mg COD/l
XI = 1149.1683 mg COD/l
XS = 113.7148 mg COD/l
XBH = 2533.1267 mg COD/l
XBA = 151.7894 mg COD/l
XP = 445.766 mg COD/l
SO = 1.3088 mg -COD/l
SNO = 8.8506 mg N/l
SNH = 11.3461 mg N/l
SND = 2.8366 mg N/l
XND = 6.8699 mg N/l
SALK = 4.924 mol HCO₃/m³
TSS = 3295.1739 mg SS/l

Reactor 1

SI = 30 mg COD/l
SS = 3.2439 mg COD/l
XI = 1149.1683 mg COD/l
XS = 98.6029 mg COD/l
XBH = 2552.1095 mg COD/l
XBA = 151.6721 mg COD/l
XP = 446.9249 mg COD/l
SO = 0.0076964 mg -COD/l
SNO = 3.5133 mg N/l
SNH = 11.8312 mg N/l
SND = 1.3621 mg N/l

XND = 6.1775 mg N/l
SALK = 5.3399 mol HCO3/m3
TSS = 3298.8583 mg SS/l

Reactor 2

SI = 30 mg COD/l
SS = 1.6707 mg COD/l
XI = 1149.1683 mg COD/l
XS = 91.7032 mg COD/l
XBH = 2552.3711 mg COD/l
XBA = 151.5303 mg COD/l
XP = 448.0839 mg COD/l
SO = 6.0271e-05 mg -COD/l
SNO = 1 mg N/l
SNH = 12.5482 mg N/l
SND = 0.78899 mg N/l
XND = 5.9537 mg N/l
SALK = 5.5706 mol HCO3/m3
TSS = 3294.6426 mg SS/l

Reactor 3

SI = 30 mg COD/l
SS = 1.2195 mg COD/l
XI = 1149.1683 mg COD/l
XS = 69.6594 mg COD/l
XBH = 2560.2025 mg COD/l
XBA = 152.6873 mg COD/l
XP = 449.6336 mg COD/l
SO = 1.635 mg -COD/l
SNO = 6.2289 mg N/l
SNH = 7.3197 mg N/l
SND = 0.8307 mg N/l
XND = 4.7131 mg N/l
SALK = 4.8236 mol HCO3/m3
TSS = 3286.0133 mg SS/l

Reactor 4

SI = 30 mg COD/l
SS = 0.97326 mg COD/l
XI = 1149.1683 mg COD/l
XS = 54.4484 mg COD/l
XBH = 2563.3104 mg COD/l
XBA = 153.7108 mg COD/l
XP = 451.1853 mg COD/l
SO = 2.4745 mg -COD/l
SNO = 11.0693 mg N/l
SNH = 2.7825 mg N/l
SND = 0.75276 mg N/l
XND = 3.8403 mg N/l
SALK = 4.1538 mol HCO3/m3
TSS = 3278.8674 mg SS/l

Reactor 5

SI = 30 mg COD/l
SS = 0.80801 mg COD/l
XI = 1149.1683 mg COD/l
XS = 44.4828 mg COD/l
XBH = 2562.8514 mg COD/l
XBA = 154.163 mg COD/l

XP = 452.7367 mg COD/l
SO = 2 mg -COD/l
SNO = 13.5243 mg N/l
SNH = 0.67193 mg N/l
SND = 0.6645 mg N/l
XND = 3.2605 mg N/l
SALK = 3.8277 mol HCO3/m3
TSS = 3272.5517 mg SS/l

Settler underflow

SI = 30 mg COD/l
SS = 0.80801 mg COD/l
XI = 2247.1366 mg COD/l
XS = 86.9837 mg COD/l
XBH = 5011.5177 mg COD/l
XBA = 301.4575 mg COD/l
XP = 885.3022 mg COD/l
SO = 2 mg -COD/l
SNO = 13.5243 mg N/l
SNH = 0.67193 mg N/l
SND = 0.6645 mg N/l
XND = 6.3757 mg N/l
SALK = 3.8277 mol HCO3/m3
TSS = 6399.2982 mg SS/l

Settler effluent

SI = 30 mg COD/l
SS = 0.80801 mg COD/l
XI = 4.39 mg COD/l
XS = 0.16993 mg COD/l
XBH = 9.7905 mg COD/l
XBA = 0.58893 mg COD/l
XP = 1.7295 mg COD/l
SO = 2 mg -COD/l
SNO = 13.5243 mg N/l
SNH = 0.67193 mg N/l
SND = 0.6645 mg N/l
XND = 0.012455 mg N/l
SALK = 3.8277 mol HCO3/m3
TSS = 12.5016 mg SS/l

Settler internal (1 is top layer)

TSS1 = 12.5016 mg SS/l
TSS2 = 18.1183 mg SS/l
TSS3 = 29.548 mg SS/l
TSS4 = 69.0015 mg SS/l
TSS5 = 356.2825 mg SS/l
TSS6 = 356.2825 mg SS/l
TSS7 = 356.2825 mg SS/l
TSS8 = 356.2825 mg SS/l
TSS9 = 356.2825 mg SS/l
TSS10 = 6399.2982 mg SS/l

Other variables

Trad. sludge age (XS + XP + XI + XBH + XBA in reactors) = 7.3273 days
Spec. sludge age (XBH + XBA in reactors and settler) = 9.139 days
Total hydraulic retention time = 15.6118 hours
Reactor hydraulic retention time = 7.8053 hours
Thickening factor at bottom of settler(TSSu/TSSfeed) = 1.9554

Thinning factor at top of settler ($TS_{\text{Seff}}/TS_{\text{Sfeed}}$) = 0.0038201

Dimensions

Reactor 1 is anoxic
Volume reactor 1 = 1000 m³
Reactor 2 is anoxic
Volume reactor 2 = 1000 m³
Reactor 3 is aerobic
Volume reactor 3 = 1333 m³
Reactor 4 is aerobic
Volume reactor 4 = 1333 m³
Reactor 5 is aerobic
Volume reactor 5 = 1333 m³
Settler height = 4 m
Settler area = 1500 m²
Settler volume = 6000 m³